

Computational Fluid Dynamics Modelling and Simulation of Laminar Convective Fluid and Heat Flow of a portable air-conditioning Unit

Part I

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Abstract— This work deals with a study on the laminar convective heat flow of a homemade air conditioning unit through a computational fluid dynamics simulation. With adoption of chilled water as the working fluid within a tube section of the evaporative compartment of the homemade air conditioner whose radius is 5mm and Height 20mm . The numerical analysis was carried out using COMSOL MULTIPHYSICS. Simulation was carried out, using $(276\text{K} (3^\circ\text{c}))$ as the inlet temperature and $293\text{K} (20^\circ\text{c})$ as the outlet temperature with a flow rate of $0.15\text{ m}^3/\text{s}$. The result showed the velocity profile of the working fluid and the temperature distribution before, during and after heat exchange, helping to achieve a Visual understanding of the Laminar convective fluid and heat flow phenomena within the cooling coil.

Index Terms—Computational Fluid Dynamics, Convection, Modelling, Simulation, Heat transfer, Comsol, Air-conditioning

1 INTRODUCTION

The home made air conditioner was designed and constructed by a Canadian Geoffrey Milburn in 2006, during the course of an extreme hot weather condition in Canada. [1]



Figure 1 Home made portable air conditioner

The evaporator unit consists basically of cooling coil primary copper $\frac{1}{4}$ " wound around a fan as shown in figure 1. The working principle, Design and construction was given detailed out in [1]

The evaporative compartment remains one of the most important parts of any cooling system unit.

The study of combined fluid flow and heat transfer inside tubes is a Fundamental problem in convective heat transfer.

Laminar convective heat transfer has found application in many works by several authors [2] [3] [4] [5] [6] [7].

Baron et al. [2] investigated the phenomenon of fully developed and developing laminar flows of a Newtonian fluid between parallel plates and through circular tubes. Sarma et al. [3] Suggested a method, to estimate the heat transfer coefficients in the entry region, of a short length of tube under developing laminar flow conditions. Zhuo et al [4]. performed 3D numerical simulations of the laminar flow and heat transfer in silicon microchannels of non-circular cross sections. Edalati et al.[8] Obtained a 41% enhancement in the convective heat transfer coefficient for a $0.8\% \text{CuO}/\text{Water}$ nanofluid after studying the heat transfer of an equilateral triangular duct.

The aim of this study is to apply numerical computation in understanding the laminar convective heat flow phenomena within the coiling coil of the home made air conditioner, with the simulation and modelling through the application of COMSOL MULTIPHYSICS.

2 GOVERNING EQUATIONS

2.1 Laminar Convective Fluid and Heat Flow

The governing equations for the laminar flow within the cooling coil are

1. Conservation of mass [continuity equation]
2. Conservation of momentum [Navier-stokes equation]
3. Conservation of Energy.

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These equations are summarized below as;

2.2 Continuity equation

$$\frac{\partial \rho}{\partial t} + \rho(\nabla \cdot \vec{v}) = 0 \tag{2.2.1}$$

$$\frac{\partial \rho}{\partial t} + \nabla(\rho \vec{v}) = 0 \tag{2.2.2}$$

$$\frac{\partial \rho}{\partial t} + \frac{\partial(\rho u)}{\partial x} + \frac{\partial(\rho v)}{\partial y} + \frac{\partial(\rho w)}{\partial z} = 0 \tag{2.2.3}$$

2.3 Navier-Stoke's Equation

$$\frac{\partial}{\partial t} [\rho \vec{v}] + \nabla \cdot (\rho \vec{v} \vec{v}) = -\nabla p - \nabla \bar{\tau} + \rho \vec{g} \tag{2.3.1}$$

$$\rho \left[\frac{\partial \vec{v}}{\partial t} + (\vec{v} \cdot \nabla) \vec{v} \right] = -\nabla p - \nabla \bar{\tau} + \rho \vec{g} \tag{2.3.2}$$

$$\rho \frac{\partial \vec{v}}{\partial t} = -\nabla p - \nabla \bar{\tau} + \rho \vec{g} \tag{2.3.3}$$

2.4 Energy Equation

$$\rho_{cp} \frac{dT}{dt} = -\nabla \cdot \vec{q} + \frac{dp}{dt} + \bar{\tau} \cdot \nabla \vec{v} \tag{2.4.1}$$

$$\rho_{cp} \left(\frac{\partial T}{\partial t} + (u \cdot \nabla) T \right) = -(\nabla \cdot \vec{q}) + \tau \cdot s - \frac{T}{\rho} \frac{\partial \rho}{\partial T} \left(\frac{\partial \rho}{\partial t} + (\mu \cdot \nabla) \rho \right) \tag{2.4.2}$$

The major mode of heat transfer under study is convection.

2.5 Newton's law of cooling

$$\dot{q}_{conv} = h[T_s - T_\infty] \quad W/m^2 \tag{2.5.1}$$

T_s = Surface temperature
 T_∞ = Temperature of the fluid

Fourier's Law of conduction

$$q = -k \frac{\partial T}{\partial x}$$

2.6 Nusselt Number N_u

$$\frac{\dot{q}_{conv}}{\dot{q}_{cond}} = \frac{h \Delta T}{k \frac{\Delta T}{L}} = \frac{hL}{k} \tag{2.5.2}$$

$$N_u = \frac{hL}{k} \tag{2.6.3}$$

3 NUMERICAL MODELS

A 3D domain which was a section of the cooling coil was created, with height 20mm and radius 5mm as shown in Figure 2 below

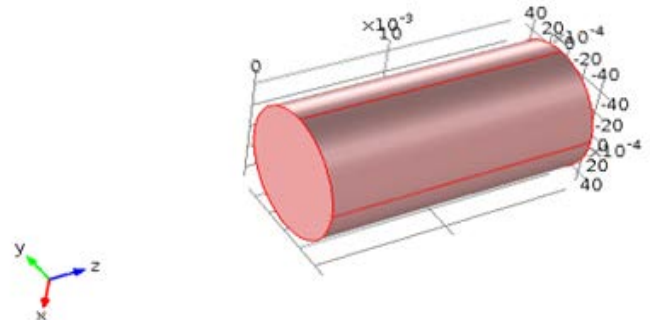


Figure 3 Schematic of the Tube section from the cooling coil

The material used for the cooling coil was copper, while the working fluid was chilled water which was considered Newtonian and incompressible.

The physics considered was conjugate Heat transfer, which was a mixture of convective heat and Laminar fluid flow.

No-slip condition was imposed at the walls of the tube.

At the inlet of the tube section, a Laminar inflow boundary condition was adopted, with a flow rate of 0.15 m³/s. At the outlet of the tube section, zero pressure condition was imposed.

An external fan was imposed at the outer of the cooling coils, to provide forced convection effect, whose static pressure curve was linear, with a free delivery flow rate of 0.01 m³/s.

3.1 Meshing

This was done using coarse free tetrahedral shape with element size ranging from 0.0014 – 0.01, refinements were done at corners with an element scale sizing factor of 0.35.

The features of the meshing are:

- Number of vertex elements: 8
- Number of edge elements: 36
- Number of boundary elements: 128
- Number of elements: 150.

The meshed tube section is shown below in Figure 3

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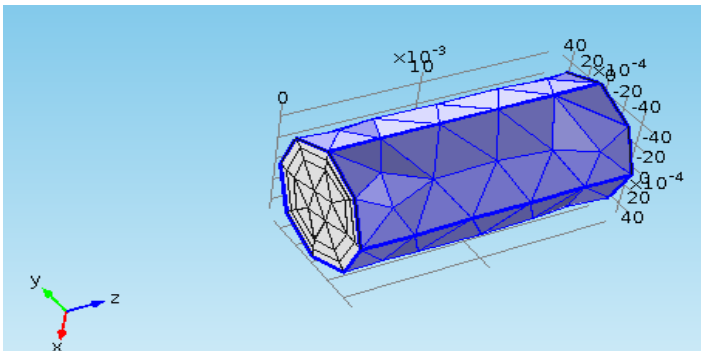


Figure 4 Meshed Tube section

4 RESULTS AND DISCUSSION

The Laminar Convective heat effect within the cooling coil is discussed. As mentioned previously the flow inside the pipe is laminar. The Velocity and Temperature profile for the fluid within the tube section was computed as shown in Figure four and Figure five below.

Figure four shows the computed velocity plot for the flow of chilled water within the tube section, as heat exchange takes place between the fluid and the ambient air with channel wall acting as an intermediary

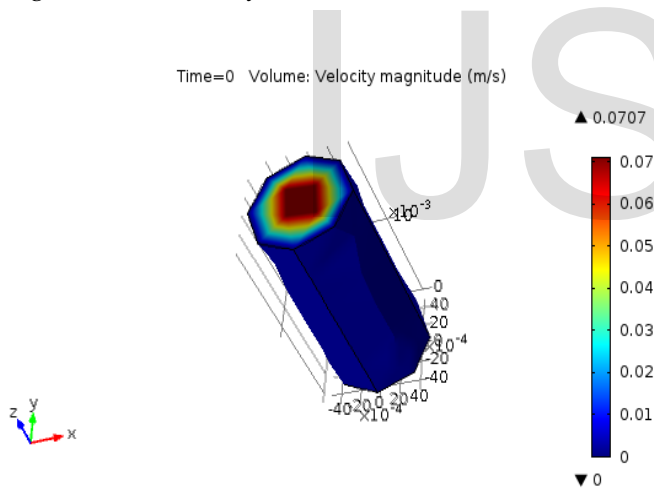


Figure 5 Velocity profile for the flow within the tube section

The temperature field obtained from the simulation is presented in Figure 5.

A cold zone is observed at the inlet of the tube section where chilled water enters. This is followed by a reduction in the temperature of the fluid at the warm zone. This happens as a temperature gradient is established between the chilled water and the ambient air surrounding the cooling coils. The exchange of heat takes place and the temperature of the working fluid increases from 276K (3°C) to 292K (19°C).

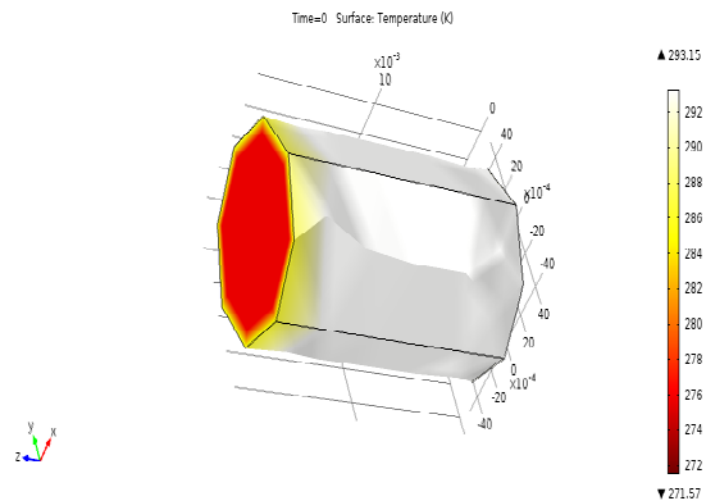


Figure 6 Temperature profile within the tube section

5 CONCLUSION

Numerical investigation of laminar convective heat and fluid flow has been investigated within a tube section, with the aid of COMSOL MULTIPHYSICS.

The inlet showed the temperature of the chilled water before heat exchange and the outlet temperature showed the temperature of the chilled water after heat exchange and energy transport.

More work still needs to be done to investigate the fluid flow and heat transfer process within the cooling coil of the evaporator. As a perspective, it would be interesting to investigate further, the pressure drop and heat transfer rate of the cooling coils, likewise also the effects of the flow rate on the heat transfer rate.

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C_p - Specific Heat Capacity ($J/(kg.k)$)

ν - Viscous Stress Tensor (Pa)

Q - Heat Source [W/m^3]

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NOMENCLATURE

CFD – Computational Fluid Dynamics

CuO – Copper(II) Oxide

ρ - Density (Kg/m^3)

U - Velocity Vector (m/s)

T - Absolute temperature (k)